#### 圆立台灣科技大學九十七學年度碩士班招生試題

1. 所組別: 化學工程系碩士班

1 目: 化工熱力學與動力學

### 總分 100 分

## Part I. 化工熱力學 (50%)

- 1. A closed system changed from state "a" to state "b" via the path  $a \to c \to b$ , as shown in Fig. 1. It was found that 250 J of heat was transferred from surroundings to the system and 200 J of work was done by the system during the changing process.
  - (a) Please calculate the amount of heat transfer  $(Q_n)$  as the system changes from state "b" to state "a" through the path  $b \to d \to a$  as illustrated in Fig. 1. During this changing process, 100 J of work is done by surroudings. You are also asked to indicate that the heat is absorbed or evolved. (5 %)
  - (b) As presented in Fig. 1, the system changes from state "a" to state "b" and then returns to state "a" via the path  $a \to c \to b \to e \to a$ . You are asked to calculate the amount of work interaction ( $W_b$ ) between the system and surroundings, if 100 J of heat is evolved from the system to surroundings during this cyclic process. Is the work done by the system or surroundings? (5 %)

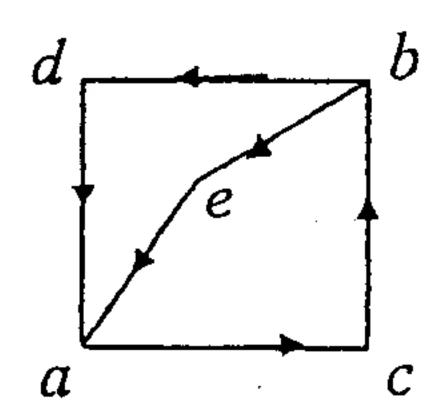


Fig. 1

- 2. Qualitatively plot a practical Rankine power cycle on a T-S diagram and indicate the constraint of each step. (5 %)
- 3. For water (1) + ethanol (2) system, its molar volume change of mixing  $(\Delta_{mix}\underline{V})$  at 300 K can be expressed by the following equation:

$$\Delta_{mix} \underline{V} \left( cm^3 / mol \right) = -x_1 x_2 \left[ 5 + 0.5(x_1 - x_2) \right]$$

where  $x_1$  and  $x_2$  are the mole fractions of water and ethanol, respectively. At 300 K, the density of pure water is 1.0 g/cm<sup>3</sup> and that of pure ethanol is 0.78 g/cm<sup>3</sup>. Now, we try to prepare 100 cm<sup>3</sup> of water + ethanol solution with the molar ratio of water : ethanol = 1 : 1 at 300 K.

- (a) Calculate the density of this aqueous solution. (5 %)
- (b) How many grams of water and ethanol are needed, respectively, to prepare the solution? (5 %)
- (c) Calculate the partial molar volume of ethanol for this solution. (10 %)
- (d) Calculate the partial molar volume of ethanol at infinite dilution. (5 %)
- 4. Describe briefly the γ-φ method for vapor-liquid equilibrium (VLE) calculation. (10 %)

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#### Part II. 化工動力學 (50%)

5. Microelectronic devices are formed by first forming SiO<sub>2</sub> on a Si waser by thermal oxidation and some procedures as illustrated in Fig. 2. The second procedure is followed by coating the SiO<sub>2</sub> with a photoresist. The pattern of the electronic circuit is then placed on the photoresist and the sample is irradiated with UV light. If the photoresist is a positive type, the sections that were irradiated with dissolve in the appropriate solvent, and those sections not irradiated will protect the SiO<sub>2</sub> from further treatment. The waser is then exposed to strong acids, such as HF, which etch the exposed SiO<sub>2</sub>. It is extremely important to know the kinetics of the reaction so that the proper depth of the channel can be achieved. The dissolution reaction is

$$SiO_2 + 6HF \rightarrow H_2SiF_6 + 2H_2O$$

(i) From the following initial rate data, determine the rate law. Also estimate the etching rate at 1 wt% of HF.

Etching rate (nm/min)	60	200	600	1000	1400
HF (wt %)	8	20	33	40	48

(ii) The etching rate may differ at various temperatures. This means that the reaction rate of a chemical reaction always follows Arrhenius behavior. Please give an example of reaction to show the transition state and the energy barrier of a reaction by using potential energy plot as a function of reaction coordinate. (15%)

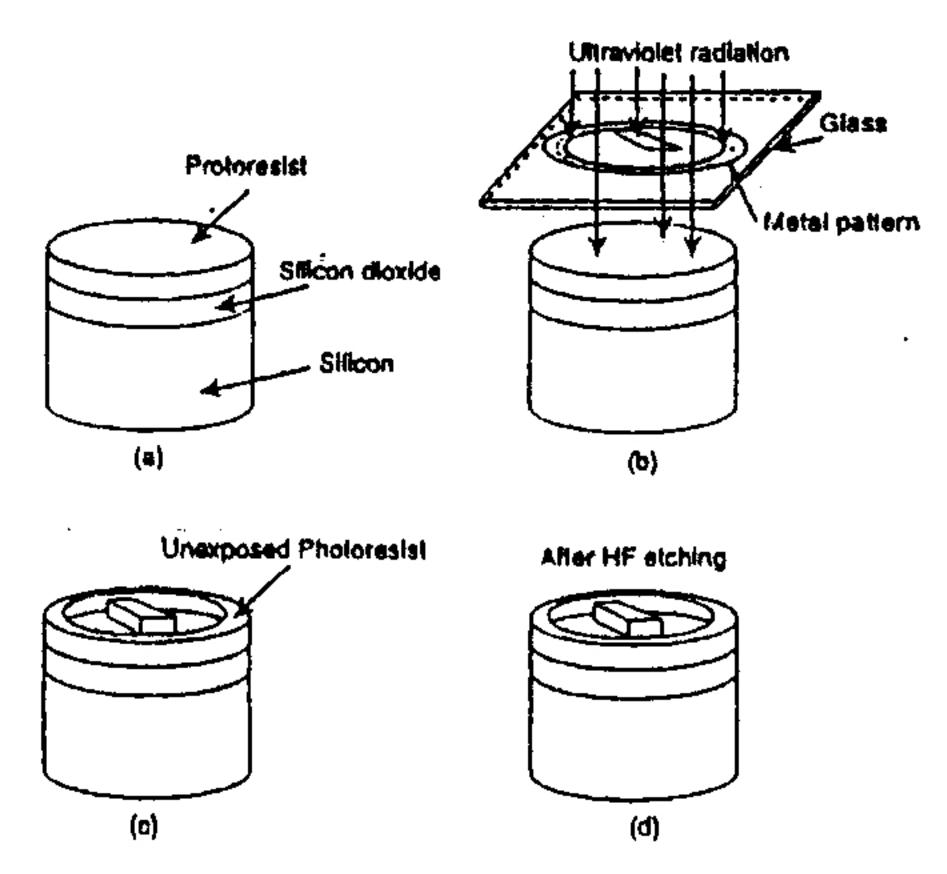


Fig. 2 Semiconductor etching

6. Chemical vapor deposition (CVD) is a technique to deposit thin films through chemical reactions of gaseous species on a solid substrate. In order to deposit PbTiO<sub>3</sub> films on Si wafers, a CVD reaction system was designed which used TEL and TTIP as the gaseous sources for Pb and Ti, respectively. Also O<sub>2</sub> was used as an oxidant. A surface reaction scheme concerning the deposition of PbTiO<sub>3</sub> is proposed as follows.

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$$TEL_{(g)} + \sigma \overset{k_1}{\underset{k_1}{\rightleftharpoons}} TEL \cdot \sigma$$
 (1)

$$\frac{1}{2}O_{2(g)} + \sigma \stackrel{k_2}{\rightleftharpoons} O \cdot \sigma \qquad (2)$$

$$TEL \cdot \sigma + 3O \cdot \sigma + TTIP_{(g)} \xrightarrow{k_3} PbTiO_{3(s)} + 4C_2H_{4(g)} + 4C_3H_{6(g)} + 4H_2O_{(g)}$$
(3)

where  $\sigma$  designates a surface adsorption site, k and k' are the rate constants for adsorption and desorption, respectively,  $k_3$  is the rate constant for PbTiO<sub>3</sub> deposition. The above reaction scheme considers an Eley-Rideal mechanism, i.e., a surface reaction among three species: two adsorbed species, TEL and dissociated oxygen, and one gaseous species TTIP, reacting to form PbTiO<sub>3</sub> films. Considering that reactions in eqs. (1) and (2) are reversible, please answer the following questions.

- (i) According to the Langmuir treatment of adsorption, please write down the rate expression for each step including adsorption and desorption using denotations of  $\theta$  (the fraction of surface adsorption site covered by the adsorbed molecules) and P (partial pressure for each species, e.g.,  $P_{TEL}$  as the partial pressure of TEL,  $P_o$ , as the partial pressure of oxygen)
- (ii) Please express the conservation equation of surface site.
- (iii) Please derive the adsorption isotherms for TEL ( $\theta_{TEL-\sigma}$ ) and dissociated oxygen ( $\theta_{O-\sigma}$ ).
- (iv) Please show that the deposition rate is linearly proportional to TTIP partial pressure but nonlinear to TEL and O<sub>2</sub> partial pressures.

  (20%)
- 7. For a reactant A proceeding the following parallel reactions:

$$A \rightarrow D$$
 (desired)

The rate expressions for each reaction are  $r_D = k_D C_A^{\alpha l}$  and  $r_U = k_U C_A^{\alpha l}$ , respectively. Please answer the following questions.

- (i) What is the total consumption rate of A?
- (ii) If the rate selectivity parameter is  $S_{DU} = r_D / r_U$ , show the relation between  $S_{DU}$  and the rate laws.
- (iii) When  $\alpha 1 \alpha 2 > 0$ , then what kind of reactor should be adopted in order to increase the growth rate of D? For the same purpose, is the concentration of reactant A should be increased or decreased? Why?

  (15%)