

國立臺灣科技大學 112 學年度碩士班招生試題

系所組別：化學工程系碩士班

科目：工程數學與輸送現象

(總分為 100 分；所有試題務必於答案卷內頁依序作答，否則不予計分)

1. (38%) A naphthalene (MW=128 g/mol) sphere is kept at a uniform temperature of 27°C and is suspended in still air at 1 atm (1×10^5 Pa) by a fine wire. The initial radius $r_1 = 2.00$ mm. The saturated vapor pressure of naphthalene at 27°C is $P_{A1} = 0.6$ mmHg, and the density of solid naphthalene is 1.14 g/cm³. The diffusivity of naphthalene in the air is 7×10^{-6} m²/s. The gas constant, R, is $8.314 \frac{\text{J}}{\text{mol}\cdot\text{K}}$.
- (10%) Derive the evaporation rate (kg/s) of naphthalene and explain the assumptions you made to simplify the governing equation.
 - (18%) Derive the profile of p_A .
 - (10%) What is the time for the completed evaporation of this naphthalene sphere?
2. (12%) Choose the CORRECT one(s) from the following descriptions.
- In a backward-feed multiple-effect evaporator, the high temperatures in the early effects reduce the viscosity, resulting in good heat and mass transfer.
 - The percentage humidity is defined as the actual vapor pressure of water in the air divided by the water vapor pressure which is saturated at the same temperature.
 - The bound moisture in solids has lower vapor pressure than water at the same temperature.
 - In the design of distillation tower, the q line represents heat condition of the feed, and q is defined as $q = (\text{molar latent heat of feed vaporization}) / (\text{heat needed to vaporize 1 mol of feed at entering conditions})$
 - The reflux of distillation increases the purity of the overhead product, and decreases the energy cost.
 - After the break-point time is reached in an adsorption bed, the solute concentration rises very rapidly, and the bed is then judged ineffective soon.
3. (30%)
- (5%) (a) In fluid mechanics, Newton's viscosity law is mainly used to describe the relationship between fluid velocity gradient and shear stress. Consider a one-dimensional flow, if the flow direction of the fluid is in the r direction, and the direction of momentum transport is in the z direction, please write the corresponding Newton's viscosity law.
 - (5%) (b) The shear stress can be regarded as the flux of which physical quantity?
 - (5%) (c) Stream function (Ψ) is useful for flow visualization. It applies to incompressible two-dimensional flow situation. For example, consider a two-dimensional x-y flow in Cartesian rectangular coordinates, we can find the relationship between (v_x, v_y) and Ψ by using continuity equation as following:



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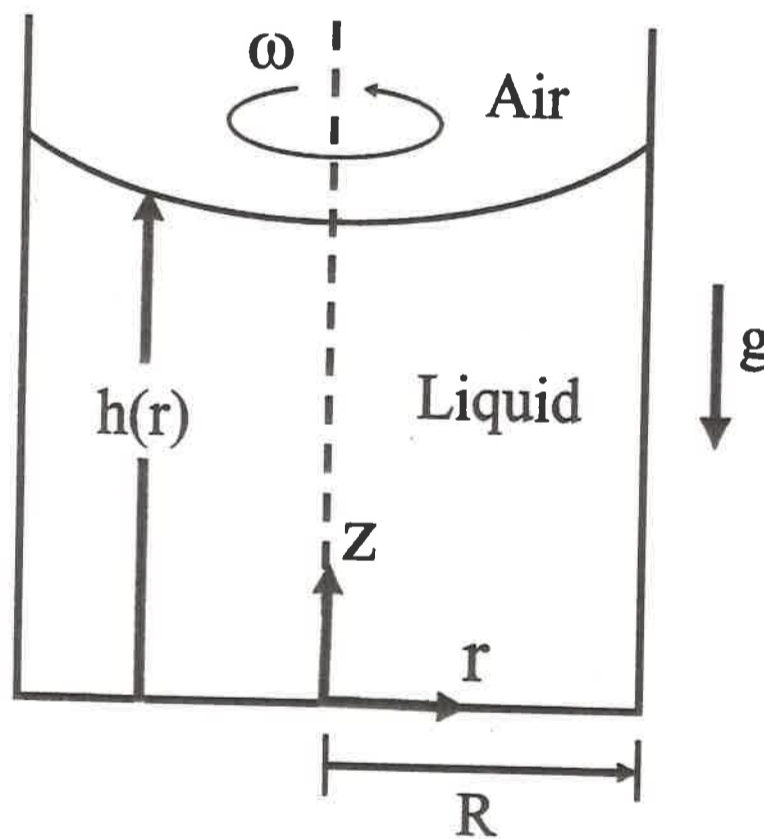
$$\therefore \nabla \cdot \vec{v} = \frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} = 0 \text{ and Let } v_x = \frac{\partial \Psi}{\partial y}$$

$$\text{substitute } v_x \text{ into } \nabla \cdot \vec{v} \Rightarrow \frac{\partial}{\partial x} \left(\frac{\partial \Psi}{\partial y} \right) + \frac{\partial v_y}{\partial y} = 0$$

$$\text{So, we can find } v_y = -\frac{\partial \Psi}{\partial x}$$

Now, we consider the flow pattern in r - θ plane of spherical coordinates. Please find the relationship between (v_r, v_θ) and Ψ .

- (15%) (d) The following figure shows a system with a gas-liquid interfaces, consisting of a liquid in an open container of radius R that is rotated at a constant angular velocity ω . Please determine the steady interface height, $h(r)$, assuming that the ambient air pressure is P_0 and the initial volume of the liquid in the tank is V_0 .



4. (20%) Please answer the following questions.

(5%) (a) Fourier law of heat conduction can be expressed as $\frac{q}{A} = -k\nabla T$. Please explain the physical meaning of negative symbol “-”.

(15%) (b) Consider a two-dimensional heat transfer in x - y plane as shown in following figure. The temperatures of the right-hand side and left-hand side are T_a and T_b , respectively. Consider the thermal conductivity, the width and the thickness of the fin are k , t_f and

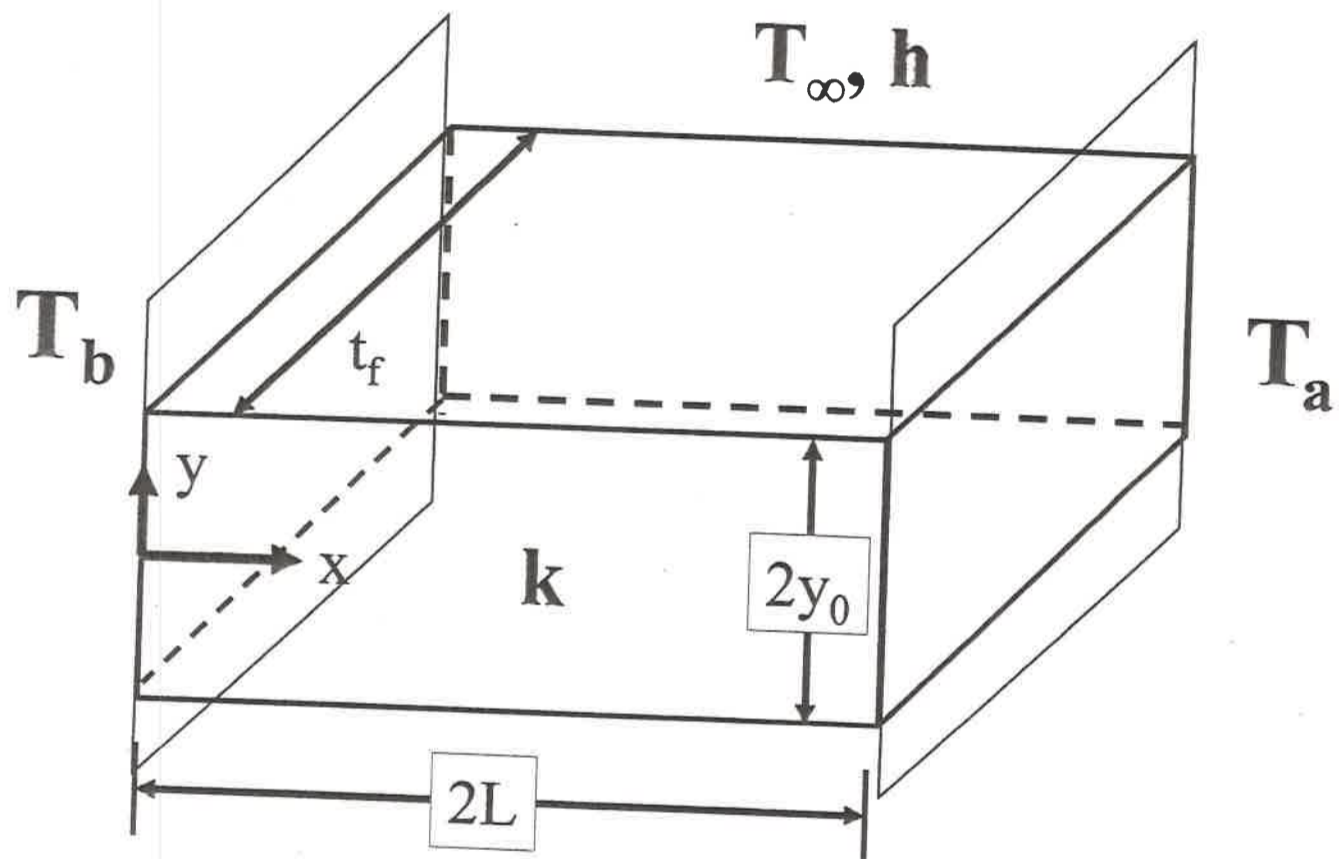
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2y₀. The temperature and heat transfer coefficient of the ambient are T_∞ and h. Please find the temperature distribution in x-y plane. [Hint: please use the definition of dimensionless temperature $\theta = \frac{T - T_b}{T_\infty - T_b}$ to solve this problem]



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Supporting materials

(a) Continuity equation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \rho \vec{v} = 0$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho v_x) + \frac{\partial}{\partial y}(\rho v_y) + \frac{\partial}{\partial z}(\rho v_z) = 0 \text{ (Cartesian rectangular coordinates)}$$

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r}(\rho r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(\rho v_\theta) + \frac{\partial}{\partial z}(\rho v_z) = 0 \text{ (Cylindrical coordinates)}$$

$$\frac{\partial \rho}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r}(\rho r^2 v_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta}(\rho v_\theta \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \phi}(\rho v_\phi) = 0 \text{ (Spherical coordinates)}$$

(b) Navier-Stokes equation

$$\rho \frac{D\vec{v}}{Dt} = -\nabla P + \mu \nabla^2 \vec{v} + \rho \vec{g}$$

Cartesian Rectangular coordinates

$$\rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{\partial P}{\partial x} + \mu \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x$$

$$\rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) = -\frac{\partial P}{\partial y} + \mu \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right) + \rho g_y$$

$$\rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \mu \left(\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z$$

Cylindrical coordinates

$$\rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} + v_z \frac{\partial v_r}{\partial z} - \frac{v_\theta^2}{r} \right) = -\frac{\partial P}{\partial r} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} + \frac{\partial^2 v_r}{\partial z^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} \right] + \rho g_r$$

$$\rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + v_z \frac{\partial v_\theta}{\partial z} + \frac{v_r v_\theta}{r} \right) = -\frac{1}{r} \frac{\partial P}{\partial \theta} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{\partial^2 v_\theta}{\partial z^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} \right] + \rho g_\theta$$

$$\rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] + \rho g_z$$

