

※ 考生請注意：本試題可使用計算機。請於答案卷(卡)作答，於本試題紙上作答者，不予計分。

**Equations**

**Navier-Stokes equation in cylindrical coordinates**

*r direction*

$$\rho \left( \frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) = -\frac{\partial P}{\partial r} + \rho g_r + \mu \left[ \frac{\partial}{\partial r} \left( \frac{1}{r} \frac{\partial}{\partial r} (r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right]$$

*\theta direction*

$$\rho \left( \frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_r v_\theta}{r} + v_z \frac{\partial v_\theta}{\partial z} \right) = -\frac{1}{r} \frac{\partial P}{\partial \theta} + \rho g_\theta + \mu \left[ \frac{\partial}{\partial r} \left( \frac{1}{r} \frac{\partial}{\partial r} (r v_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} + \frac{\partial^2 v_\theta}{\partial z^2} \right]$$

*z direction*

$$\rho \left( \frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \rho g_z + \mu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right]$$

**Shear stress components in cylindrical and spherical coordinates**

$$\begin{aligned} \tau_{r\theta} = \tau_{\theta r} &= \mu \left[ r \frac{\partial}{\partial r} \left( \frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right] & \tau_{r\theta} = \tau_{\theta r} &= \mu \left[ r \frac{\partial}{\partial r} \left( \frac{v_\theta}{r} \right) + \frac{1}{r} \frac{\partial v_r}{\partial \theta} \right] \\ \tau_{z\theta} = \tau_{\theta z} &= \mu \left[ \frac{\partial v_\theta}{\partial z} + \frac{1}{r} \frac{\partial v_z}{\partial \theta} \right] & \tau_{\phi\theta} = \tau_{\theta\phi} &= \mu \left[ \frac{\sin \theta}{r} \frac{\partial}{\partial \theta} \left( \frac{v_\phi}{\sin \theta} \right) + \frac{1}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} \right] \\ \tau_{rz} = \tau_{zr} &= \mu \left[ \frac{\partial v_z}{\partial r} + \frac{\partial v_r}{\partial z} \right] & \tau_{\phi r} = \tau_{r\phi} &= \mu \left[ \frac{1}{r \sin \theta} \frac{\partial v_r}{\partial \phi} + r \frac{\partial}{\partial r} \left( \frac{v_\phi}{r} \right) \right] \end{aligned}$$

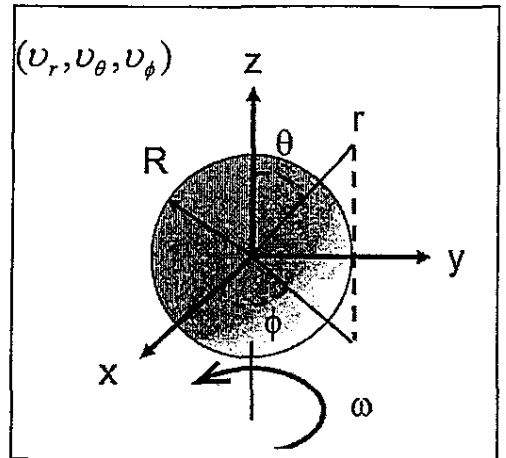
**Vorticity in spherical coordinates**

$$\nabla \times \vec{v} = \left( \left[ \frac{1}{r \sin \theta} \left[ \frac{\partial}{\partial \theta} (v_\phi \sin \theta) - \frac{\partial v_\phi}{\partial \phi} \right] \right) \vec{e}_r + \left( \frac{1}{r \sin \theta} \frac{\partial v_r}{\partial \phi} - \frac{1}{r} \frac{\partial}{\partial r} (r v_\phi) \right) \vec{e}_\theta + \frac{1}{r} \left( \frac{\partial}{\partial r} (r v_\theta) - \frac{\partial v_r}{\partial \theta} \right) \vec{e}_\phi \right)$$

**Questions**

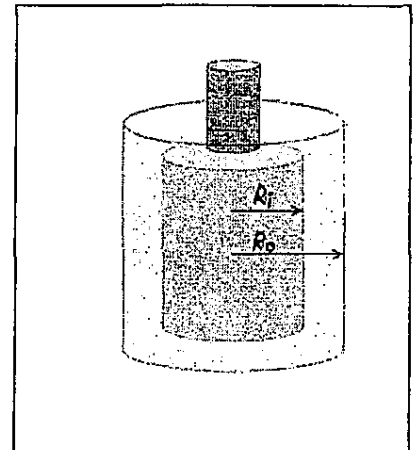
1. Consider a solid sphere of radius  $R$  rotating in a large body of a stagnant, incompressible Newtonian fluid as shown on the right. Assume that the fluid flow is laminar and steady. Assume no effect of gravity and pressure. The velocity was found to be

$$\vec{v} = (R^3 \omega / r^2) \sin \theta \vec{e}_\phi$$



- (a) Derive the surface velocity at  $\theta = 45^\circ$ . (2%)
- (b) Derive all the components of the shear stress as a function of  $r$  and  $\theta$ . (4%)
- (c) Derive the shear stress that the rotating sphere acts on the fluid at  $\theta = 45^\circ$ . Please specify the direction (4%)
- (d) Derive the vorticity on the sphere. (4%)

2. The right figure shows the geometry of a rheological experiment (**Stormer viscometer**). A fluid lies between an outer cylinder  $R_o$  (18.0 mm) and an inner cylinder  $R_i$  (17.0 mm). The inner cylinder is rotated at 4000 rpm. A torsion meter was installed on the outer cylinder and torque is measured to be 0.05 Nm. The length of the inner cylinder is 36 mm. Assume that the fluid is incompressible and Newtonian. And the viscous end effects are negligible. No-slip condition was applied on the solid surface.



- (a) Write down the simplified Navier-Stokes equation and derive that the velocity is  $\vec{v} = (C_1/r + C_2 r) \vec{e}_\theta$ , where  $C_1$  and  $C_2$  are constants. (6%)
- (b) Write down the boundary conditions and determine the constants,  $C_1$  and  $C_2$ . (4%)
- (c) Explain how to determine the fluid viscosity and calculate it. (6%)

3. Explain the following: (10%)

- (a) Nusselt number
- (b) A lumped-parameter system (in unsteady state heat conduction)
- (c) Decrease of the heat flux after nucleate boiling during pool boiling
- (d) Heat exchanger effectiveness
- (e) Stefan-Boltzmann Law (in thermal radiation)

4. An insulated cylindrical pipe with length  $L$  is shown in the following. Consider one-dimension heat transfer through cylindrical layers,

- (a) Derive the thermal resistance of the pipe. (7%)  
 (b) Find the critical radius of insulation. (8%)

The inner radius of the pipe:  $r_1$

The outer radius of the pipe:  $r_2$

The outer radius of the insulation:  $r_3$

The thermal conductivity of the pipe:  $k_1$

The thermal conductivity of the insulation material:  $k_2$

The temperature of inner wall of the pipe:  $T_1$

The temperature of outer wall of the pipe:  $T_2$

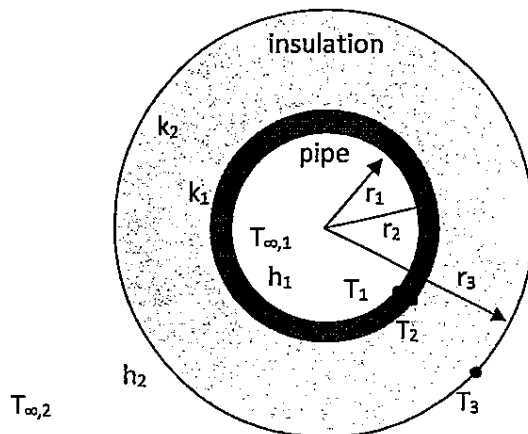
The temperature of outer surface of the insulation:  $T_3$

The temperature inside the pipe:  $T_{\infty,1}$

The temperature outside the insulation:  $T_{\infty,2}$

The heat transfer coefficient at inner surface of the pipe:  $h_1$

The heat transfer coefficient at outer surface of the insulation:  $h_2$



5. Two large tanks contain a mixture of  $N_2$  and  $O_2$ , but at different concentrations. Tank A has 80 mole percent  $N_2$  and 20 mole percent  $O_2$ , while Tank B has 15 mole percent  $N_2$  and 85 mole percent  $O_2$ . The volumes of Tank A and Tank B are 20 and 40  $m^3$ , respectively. A tube with a length of 2.0 m and an inside diameter of 0.10 m connects the two tanks. Assume that the pressure is 1 atm and the temperature is 25  $^{\circ}C$ .

- (a) By using the differential control-volume concept, derive the general expression for the flux of  $N_2$  between the two tanks as a function of the partial pressure of  $N_2$ . List all the assumptions you made to obtain the  $N_2$  flux. (12%)  
 (b) The diffusion coefficient of  $N_2$  in  $O_2$  is  $2.0 \times 10^{-5} m^2/s$  at the given conditions. Calculate the rate of  $N_2$  diffusion between the tanks. (4%)  
 (c) By the use of the "film concept" for mass transfer, find the convective mass-transfer coefficient. (4%)

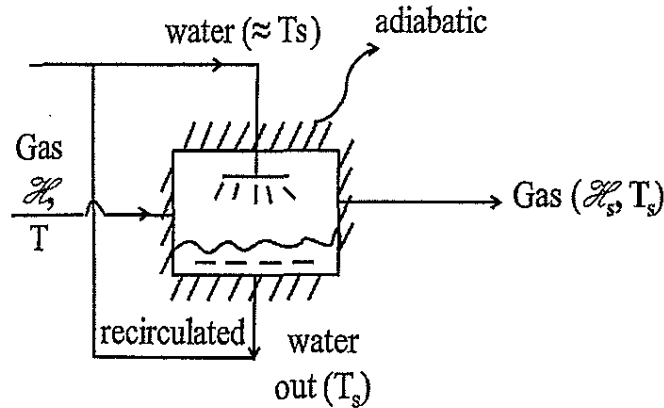
6. (a) In an adiabatic saturator shown below, a liquid was sprayed into a stream of gas. The input gas, with an initial humidity  $\mathcal{H}$  and temperature  $T$ , was cooled and get equilibrium with the liquid. The exit temperatures of liquid and gas are all  $T_s$  (termed as *adiabatic saturation temperature*) and the humidity of the leaving gas becomes saturated ( $\mathcal{H}_s$ ). The remaining liquid was recirculated to the spray nozzle. Please derive the following equation (8%)

$$\frac{\mathcal{H}_s - \mathcal{H}}{T - T_s} = \frac{C_s}{\lambda_s}$$

Where

$C_s$ : humid heat capacity

$\lambda_s$ : latent heat of water at  $T_s$



(b) If the temperatures of the input ( $T$ ) and output ( $T_s$ ) gases can be measured, how to measure the **humidity** and **web-bulb temperature** of the input gas by humidity chart? Drawing a simple figure to describe your answer. (7%)

7. A gas stream contains 50% (in mole percent) acetone and 50% air. The acetone is to be removed by adsorption into a nonvolatile oil. The entering oil contains 1% acetone. The equilibrium relationship of acetone concentration in the air ( $y$ ) and oil ( $x$ ) is  $y = 2x$ . If one would like to remove 96% of the acetone from the entering gas, what is the minimum flow rate of the entering oil ( $L_a$ ) per 100 mole of entering gas? What is the number of ideal stages required in this condition? (10%)

