

# 大同大學 104 學年度研究所碩士班入學考試試題

考試科目：熱力與動力

所別：化學工程研究所(甲組)

第 1/1 頁

註：本次考試 不可以參考自己的書籍及筆記； 不可以使用字典； 可以使用計算器。

1. [15%] Translate each of the following terms into Chinese and explain it briefly:

- 1.1 Equation of State.
- 1.2 Isenthalpic Process.
- 1.3 Isolated System

2. [20%] The following equation is reasonably good for estimating the heat of vaporization,  $\Delta H^{\text{vap}}$  (J/mol), and vapor pressure,  $P^{\text{vap}}$  (bar), over small temperature ranges:

$$\ln(P^{\text{vap}}/C) = -\Delta H^{\text{vap}}/RT$$

where  $T$  is the temperature in Kelvin and  $C$  is a constant in bar. Given that the vapor pressure of water at  $120^\circ\text{C}$  is 1.985 bar, estimate the average heat of vaporization (in J/mol) between  $100^\circ\text{C}$  and  $120^\circ\text{C}$ , and the vapor pressure (in bar) of water at  $110^\circ\text{C}$ . Note that the vapor pressure of water at its boiling point is 1 atm.

3. [15%] An expression for  $d\underline{S}$  is given below:

$$d\underline{S} = \frac{C_v}{T} dT + \left(\frac{\partial P}{\partial T}\right)_V dV = \frac{C_p}{T} dT - \left(\frac{\partial V}{\partial T}\right)_P dP$$

where  $\underline{S}$  is molar entropy. Derive an expression of  $\Delta\underline{S}$  [ $\underline{S}_2(T_2, V_2) - \underline{S}_1(T_1, V_1)$ ] in terms of  $T_1$ ,  $V_1$ ,  $T_2$  and  $V_2$  for an ideal gas, and then calculate the entropy change (in J/K) for 5 moles of ideal gas subject to a state change from ( $300^\circ\text{C}$ ,  $0.0500 \text{ m}^3/\text{mol}$ ) to ( $600^\circ\text{C}$ ,  $0.0300 \text{ m}^3/\text{mol}$ )? Note that  $R = 8.314 \text{ J/mol/K}$ ,  $C_v = 2.5R$ .

4. [20%] Derive the governing equation for the PFR on a reactor system shown in Figure (1) based on (a) the general mole balance equation and (b) the shell balance equation.

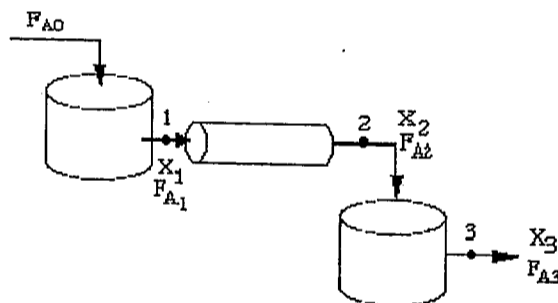


Figure (1)

5. [20%] The adiabatic exothermic irreversible gas-phase reaction  $2A + B \rightarrow 2C$  is to be carried out in a flow reactor for an equimolar feed of A and B.

$$\frac{F_{A0}}{-r_A} (\text{m}^3) = 5 \times 10^5 - 8 \times 10^5 \cdot X \quad \text{for } 0 \leq X \leq 0.5;$$

$$\frac{F_{A0}}{-r_A} (\text{m}^3) = 1 \times 10^5 + 1 \times 10^6 \cdot (X - 0.5) \quad \text{for } 0.5 \leq X \leq 0.9.$$

What PFR volume is necessary to achieve 70% conversion?

If there is a CSTR ( $9 \times 10^4 \text{ m}^3$ ) + PFR ( $6.5 \times 10^4 \text{ m}^3$ ) reactor system, what conversion can be achieved at the exit of the CSTR and the PFR respectively? (20%)

6. [10%] The 2nd order reaction  $A+B \rightarrow C$  ( $-r_A = kC_A^2$ ) is carried out in a continuous stirred reactor in which the volumetric flow rate,  $v$ , is constant. Determine the reactor volume necessary to reduce the exiting concentration to 20% of the entering concentration given that the volumetric flow rate is  $10 \text{ dm}^3/\text{min}$ ; the concentration is  $1 \text{ mol/dm}^3$  and the specific reaction rate,  $k$ , is  $0.23 \text{ dm}^3/(\text{min} \cdot \text{mol})$ .