

# 國立中山大學 104 學年度碩士暨碩士專班招生考試試題

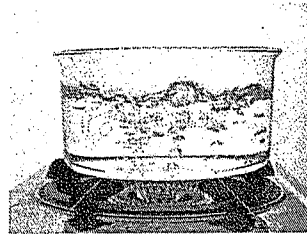
科目名稱：基礎熱傳學【機電系碩士班甲組】

題號：438003

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1. 25%. A pot filled with water of 1.2 kg is put on a stove. With a heating power set to 1.25 kW, the water is heated up from 25 °C. Please use your knowledge of thermodynamics to answer the questions below.



(<http://iab-sciencelab.wikispaces.com/>)

(a)(7%) The first law of thermodynamics for transient processes is listed below:

$$\dot{Q}_{1-2} - \dot{W}_{1-2} + \sum \dot{m}_i h_i - \sum \dot{m}_o h_o = \dot{m}_2 \left( u_2 + \frac{1}{2} V_2^2 + gZ_2 \right) - \dot{m}_1 \left( u_1 + \frac{1}{2} V_1^2 + gZ_1 \right) \quad (\text{Eq. 1.1})$$

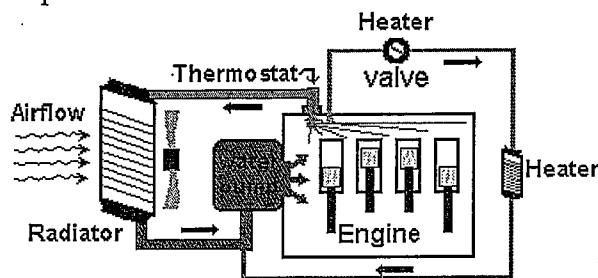
$\dot{Q}_{1-2}$  and  $\dot{W}_{1-2}$  are heat transfer into the system and work done by the system during the transient process from state 1 to 2.  $\dot{m}$  and  $h$  are the mass flow rate and enthalpy. The subscript  $i$  and  $o$  represent for inlet and outlet of the system.  $u$ ,  $V$ , and  $Z$  represent the internal energy, velocity, and elevation. You are asked to determine the time taken to heat the water from 25 °C to a certain temperature degree, how do you **simplify** Equation 1.1, which allows you to deal with the problem?

(b)(7%) How do you further relate your simplified equation in (a) to the water temperature? The purpose is to make this simplified equation in (a) as a function of the water temperature.

(c)(7%) If the specific heat ( $C_p$ ) of water is known (4.18 kJ/kg-K) for the working temperature, how do you rearrange your simplified equation in (b) to calculate the total time taken to heat up the water?

(d)(4%) After how long time do you expect the water temperature to be 100 °C?

2. 25%. An engine coolant at 60 °C enters an engine and removes engine heat around 19 kW when leaving the engine, the coolant cannot exceed a specific temperature. Please use your knowledge of thermodynamics to answer the questions below:



(<http://intecsciwri.wikidot.com/internal-combustion-engine>)

(a)(7%) You are asked to determine the required mass flow rate of the coolant, how do you simplify Eq. (1.1), which allows you to deal with the problem?

(b)(7%) How do you further relate your simplified equation in (a) to the coolant temperature? The purpose is to make this simplified equation in (a) as a function of the coolant temperature.

(c)(7%) If the specific heat ( $C_p$ ) of coolant is known (2.42 kJ/kg-K) for the working temperature, how do you rearrange your simplified equation in (b) to calculate the required mass flow rate of the coolant?

(d)(4%) What is the required mass flow rate if the coolant should come out at maximum 95 °C?

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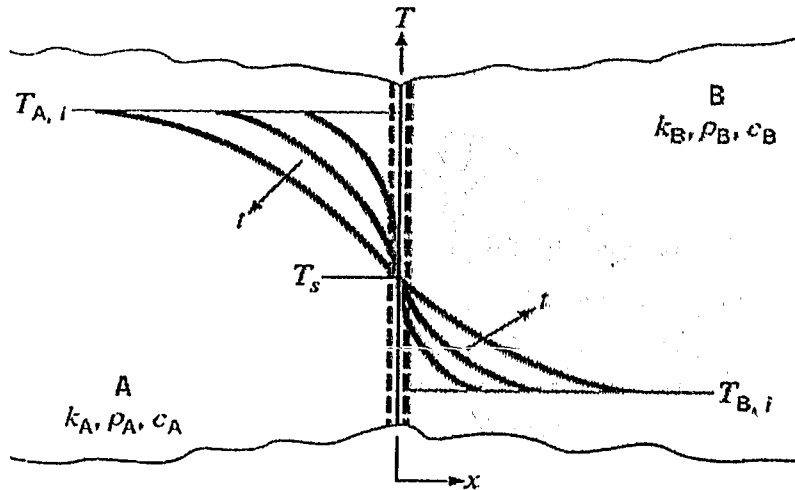
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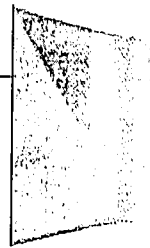
3.20%. Two semi-infinite solids A and B with uniform initial temperature  $T_{A,i}$  and  $T_{B,i}$  are placed side by side at  $x=0$  from  $t>0$  as shown in the figure. The thermal conductivity, density, heat capacity of solid A and B can be denoted as  $(k_A, \rho_A, c_A)$  and  $(k_B, \rho_B, c_B)$ . The temperature profile  $T(x, t)$  is illustrated in the figure. As time  $t$  increases, the temperature difference between these two solids will decrease. The temperature  $T$  at  $x=0$  will be independent of time  $t$ . Please calculate the temperature  $T$  at  $x=0$ .



Hint: When a single semi-infinite solid with initial condition  $T_i$  is suddenly imposed by a constant temperature  $T_s$  at  $x=0$ , the heat flux  $q_s'$ , which is a function of time  $t$ , can be expressed as following equation:

$$q_s''(t) = k(T_s - T_i) / (\pi \alpha t)^{1/2}$$

$$\begin{aligned} T(x, 0) &= T_i \\ T(0, t) &= T_s \end{aligned}$$



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4.(25%) Consider a two-dimensional square solid in Figure 4.1 with length defined as  $L$  and a uniform initial temperature  $T_0$ . Then the upper side is suddenly imposed by a constant temperature  $T_1$ . The steady state temperature  $T(x,y)$  can be solved by the following heat equation and boundary conditions in Equation 4.1. The solution  $T(x,y)$  is already given below as Equation 4.2:

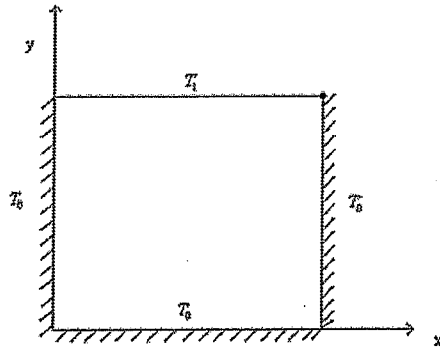


Figure 4.1

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} = 0 \quad (\text{Eq. 4.1})$$

$$BC'S : T(x, 0) = T_0, \quad T(0, y) = T_0, \quad T(L, y) = T_0, \quad T(x, L) = T_1$$

$$\Rightarrow \frac{T(x, y) - T_0}{T_1 - T_0} = \frac{2}{\pi} \sum_{n=1}^{\infty} \frac{(-1)^{n+1} + 1}{n} \cdot \sin\left(\frac{n\pi x}{L}\right) \cdot \frac{\sinh\left(\frac{n\pi y}{L}\right)}{\sinh(n\pi)} \quad (\text{Eq. 4.2})$$

(a)(10%) Now please consider a flow inside a channel. The representative cross section is shown in Figure 4.2. The channel has a constant cross-sectional area along  $z$  axis. The cross section is a square with length  $L$ . Initially, the flow inside the channel is stationary. Then the upper side of the channel is moving at a constant velocity  $U_1$  along  $z$  axis while the other three side walls remain stationary.

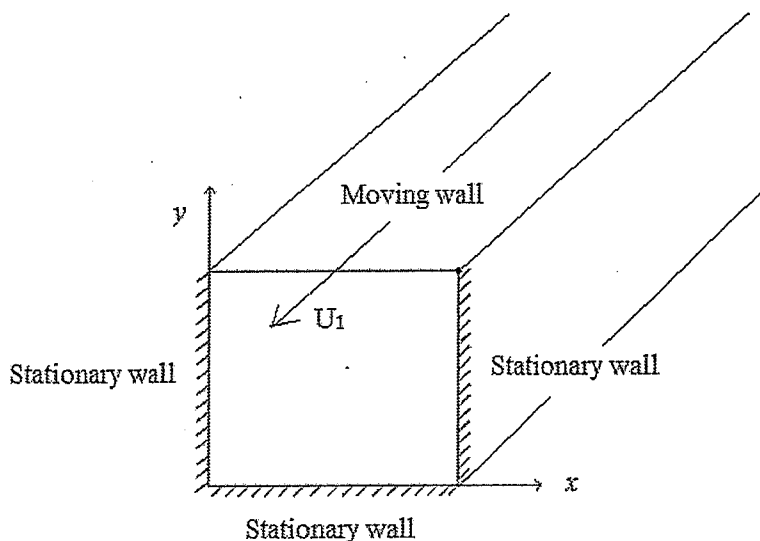


Figure 4.2

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The z momentum equation of Figure 4.2 is given as Equation 4.3:

$$\frac{\partial u_z}{\partial t} + u_x \frac{\partial u_z}{\partial x} + u_y \frac{\partial u_z}{\partial y} + u_z \frac{\partial u_z}{\partial z} = -\frac{\partial p}{\partial z} + \mu \left( \frac{\partial^2 u_z}{\partial x^2} + \frac{\partial^2 u_z}{\partial y^2} + \frac{\partial^2 u_z}{\partial z^2} \right) \quad (\text{Eq. 4.3})$$

Assume the flow is fully-developed in z direction, steady, incompressible, laminar, and **WITHOUT** pressure gradient. Also,  $u_x$  and  $u_y$  in x and y direction can be neglected. Please simplify Equation 4.3.

(b)(5%) Please list velocity boundary conditions of  $u_z$  in z direction for these four side walls.

(c)(10%) Comparing your results of (a) and (b) to Equation (4.1), then please utilize Equation (4.2) to give solution of  $u_z(x,y)$  of Figure 4.2.

5.(5%) The thermal resistance is defined as the ratio of the temperature difference to the heat transfer rate. Similarly, flow resistance of a pipe flow can be defined as the ratio of the pressure drop to the volume flow rate. The volume flow rate  $Q$  can be obtained by pressure drop  $\Delta p$  of the pipe over a distance  $L$ , fluid viscosity  $\mu$ , and the diameter  $R$  of the pipe. can be derived as following:

$$Q = \frac{\pi R^4 \Delta p}{8 \mu L}$$

The flow resistance  $F$  then becomes:

$$F \equiv \frac{\Delta p}{Q} = \frac{8 \mu L}{\pi R^4} \quad (\text{Eq. 5.1})$$

Recently, the mayor of Taipei City, Ko Wen-Je (柯文哲), has questioned the design of the underground passage of the Taipei Dome (台北巨蛋). From the entrance to the exit, the diameter of the underground passage varies from 80 to 6 meter. Please comment how his concern comes from by Equation 5.1. Can Equation 5.1 really applied to this design problem? Why?