國立雲林科技大學 系所:化材系 101 學年度碩士班暨碩士在職專班招生考試試題 科目:單元操作與輸送現象

1. A liquid flows through a capillary with an inside radius $R=10^{-3}$ m and a length L=0.4 m. The viscosity of the liquid is 1.5×10^{-3} Pa·s. The velocity distribution inside the capillary is

$$v = 0.3 \left[1 - \left(\frac{r}{R} \right)^2 \right]$$
 m/s, where *r* is the radial coordinate

- (a) What is the volumetric flow rate? (10%)
- (b) What is the pressure drop Δp across the capillary during flow? (10%)

Hint: the flux of r-momentum in the flow direction $\tau = \frac{\Delta p}{2L}r$

- 2. An oil with heat capacity c_p = 2.5 kJ/kg · K is flowing through a double-pipe heat exchanger at a rate of 7500 kg/h and is to be cooled from 373 K to 343 K. Cooling water (c_p = 4.187 kJ/kg · K) entering at 298 K and flowing **counterflow** at a rate of 3500 kg/h is available.
 - (a) Calculate the outlet temperature of the cooling water (5%)
 - (b) Calculate the overall heat transfer coefficient in $W/m^2 \cdot K$ if the heat-transfer area inside the heat exchanger is 6.5 m² (10%)
- 3. A Newtonian fluid is confined between two parallel infinite plates with a distance B apart. The lower plate is moving leftward at a constant velocity v_0 and the upper plate is moving rightward at a constant velocity $2v_0$. The pressure gradient in the flow is $\frac{P_0 - P_L}{L}$ Assuming that the flow is steady-state and laminar and gravity is negligible, find the velocity distribution (15%)



- 4. 利用逆流式套管熱交換器(countercurrent double-pipe heat exchanger),以 105 ℃ 凝結水蒸汽(condensing steam)將空氣自 30 °C 加熱至 80 °C。假設主要熱傳阻 力控制在空氣熱對流部份。已知空氣熱對流的熱傳係數(h)經驗式為 *Nu* = 0.023 Re^{0.8} Pr^{0.4},式中 Nu 為納瑟數(Nusselt number)、Re 為雷諾數 (Reynolds number)、Pr 為普蘭多數(Prandtl number)。若改用 120 °C 凝結水蒸 汽加熱空氣同樣自 30 °C 加熱至 80 °C,試問所加熱空氣的流量為原所加熱 空氣流量的多少倍? (15 分)
- 5. 有一液珠懸浮於靜止不動氣體中,液珠成分為A,氣體為A和B。若B不溶於A,而A自液珠表面蒸發,然後擴散至氣相中。因液珠很小可視為球狀, 假設液體之蒸發速率緩慢,液珠的半徑R可視為不變。試推導出計算液珠 蒸發速率的方程式。(20分)
- 6. 在298K及1atm下,一填料塔(packing tower)中利用有機胺溶液吸收二氧化碳。
 氣體進入時含1.26 mol%的二氧化碳,離去時含0.04 mol%。假設在操作條件範圍,二氧化碳與有機胺溶液間平衡關係遵守亨利定律(Henry's law),亦
 即 y_{C02}=1.575x_{C02}。氣體流速為2.3 g-mol/s,液體流速為4.8 g-mol/s。已知填料塔直徑為40 cm,總體質傳係數(overall mass transfer coefficient)與單位
 體積的表面積的乘積 K_ya 為 5.0 x 10⁻⁵ mol/(cm³-s),試計算填料塔高為多少m? (15分)